

BITS, PILANI-DUBAI, ACADEMIC CITY, DUBAI Second SEMESTER 2007-2008

CHE C221 Chemical Process Calculations

Comprehensive Examination (SOLUTION) (Closed Book)

DURATION: 3 Hours

DATE: 01-06-02008 MAXIMUM MARKS: 120

Note: Attempt ALL questions. Draw a labeled flow diagram wherever necessary, mentioning therein all the known and unknown variables. Write all assumptions and steps clearly.

Question 1 Write brief and to-the-point answers to the following questions. Answer all the parts together and in sequence.

(a)	Define selectivity and yield.	[2+2]
(b)	How standard atm (a unit of pressure) is related to psi and bar?	[2]
(c)	Differentiate between fresh feed and process feed?	[2]
(d)	How is specific gravity defined for liquids and for gases?	[2+2]
(e)	What are the assumptions made in calculating the average molecular	weight of
	air?	[2]
(f)	How are absolute saturation and relative saturation related? Write the	formula
	relating the two.	[2]
(g)	What is the difference between higher heating value (HHV) and lower	heating
	value (LHV) of a fuel?	[2]

(h) How mixing of real solutions differs from that of ideal solutions in terms of energy considerations? [2]

Solution: Consult class notes.

Question 2

A polymer blend is to be formed from the three compounds whose compositions and approximate formulas are listed in the table below. Determine the percentages of each compound A, B, and C to be mixed in a mixture to achieve the desired composition D. [10]

	Compound (%)			
Composition	A	В	С	Desired mixture, D
$(CH_4)_x$	25	35	55	30
$(C_2H_6)_x$	35	20	40	30
$(C_{3}H_{8})_{x}$	40	45	5	40
Total	100	100	100	100

Solution:

Basis: 1 kg-mol of mixture. Let a, b, and c be the kg-mol of each mixture; these are unknowns. Equations: 0.25 a + 0.35 b + 0.55 C = 0.300.35 a + 0.20 b + 0.40 c = 0.300.40 a + 0.45 b + 0.05 c = 0.40Solving above equations simultaneously, **a** = 0.60, **b** = 0.35, **c** = 0.05.

Question 3

In a process for the manufacture of chlorine by direct oxidation of HCl with air over a catalyst to form Cl_2 and H_2O (only), the exit product is composed of HCl (4.4%), Cl_2 (19.8%), O_2 (4.0%), and N_2 (52.0%). What is

- (a) the limiting reactant,
- (b) the percent excess reactant,
- (c) The degree of completion of reaction?

[10]

Solution:

4 HCl + $O_2 \rightarrow 2 \text{ Cl}_2 + 2 \text{ H}_2\text{O}$

Component	<u>mol %</u>
HCI	4.4
Cl ₂	19.8
H₂O	19.8
O ₂	4.0
<u>N₂</u>	52.0
Total	100.0

Entering moles	
<u>HCI</u>	<u>O2</u>
44	4 0

	4.4	4.0
<u>2 X 19.8</u>	= 39.6	19.8/2 = 9.9
Total	44.0	13.9

- a) So, HCl is the limiting reactant.
- b) % excess = [13.9 (44.0/4)]/(44.0/4) * 100 = 26.36%
- c) % completion = (44 4.4)/44 100 = **90%**

Question 4

(a) A synthesis gas analyzing 6.4% CO₂, 0.2% O₂, 40.0% CO, and 50.8% H₂, (the balance is N_2), is burned with 40% dry excess air. What is the composition of the flue gas? [15]

Solution:

Basis: 100 kg-mol

	<u>i caccion</u>	$reqa. U_2$	CO_2	H ₂ O	N ₂	O ₂
6.4			6.4			<u> </u>
0.2		- 0.2				
40.0 C	$0 + \frac{1}{2} O_2 \rightarrow CO_2$	20.0	40.0			
50.8 H	$_2 + \frac{1}{2} O_2 \rightarrow H_2 O$	25.4		50.8		
2.6					2.6	
cess O ₂ : (0.40	0)(45.2)	18.08				18.08
tal O ₂ in $=$		63.28				
in with $O_2 =$	(63.28)(79/21) =			238.0)5	
tals		-	46.4	50.8	240.	65 18.1
•	$\begin{array}{c} 6.4 \\ 0.2 \\ 40.0 C \\ 50.8 H \\ 2.6 \\ cess O_2: (0.40 \\ tal O_2 in = \\ in with O_2 = \\ otals \\ \end{array}$	$\begin{array}{ccccc} 6.4 & & & & \\ 0.2 & & & & \\ 40.0 & CO + \frac{1}{2} & O_2 \rightarrow CO_2 \\ 50.8 & H_2 + \frac{1}{2} & O_2 \rightarrow H_2O \\ 2.6 & & & \\ cess & O_2: (0.40)(45.2) \\ tal & O_2 & in = \\ in with & O_2 = (63.28)(79/21) = \\ \text{otals} \end{array}$	6.4 0.2 - 40.0 $CO + \frac{1}{2}O_2 \rightarrow CO_2$ 20.0 50.8 $H_2 + \frac{1}{2}O_2 \rightarrow H_2O$ 25.4 2.6 cess O_2 : (0.40)(45.2) 18.08 tal O_2 in = 63.28 in with O_2 = (63.28)(79/21) =	6.4 6.4 0.2 6.4 40.0 $CO + \frac{1}{2}O_2 \rightarrow CO_2$ 20.0 40.0 50.8 $H_2 + \frac{1}{2}O_2 \rightarrow H_2O$ 25.4 25.4 2.6 cess O_2: (0.40)(45.2) 18.08 63.28 in with $O_2 = (63.28)(79/21) =$ 46.4	6.4 6.4 0.2 - 6.4 40.0 $CO + \frac{1}{2}O_2 \rightarrow CO_2$ 20.0 40.0 50.8 $H_2 + \frac{1}{2}O_2 \rightarrow H_2O$ 25.4 50.8 2.6 cess $O_2:$ $(0.40)(45.2)$ 18.08 tal O_2 in = 63.28 in with $O_2 = (63.28)(79/21) =$ 238.0 otals 46.4 50.8	6.4 6.4 0.2 6.4 40.0 CO + $\frac{1}{2}$ O ₂ \rightarrow CO ₂ 20.0 40.0 50.8 H ₂ + $\frac{1}{2}$ O ₂ \rightarrow H ₂ O 25.4 50.8 2.6 2.6 cess O ₂ : (0.40)(45.2) 18.08 63.28 tal O ₂ in = 63.28 46.4 50.8 240. otals 46.4 50.8 240.

Comp.	mol	%
CO ₂	46.4	13.0
H₂O	50.8	14.3
N ₂	240.65	67.6
<u>O₂</u>	18.1	5.1
Totals	356.0	100

(b) Metallurgical-grade silicon is purified to electronic grade for use in semiconductor industry by chemically separating it from its impurities. The Si metal reacts in varying degrees with hydrogen chloride gas at 300 °C to form several polychlorinated silanes. Trichlorosilane is liquid at room temperature and is easily separated by fractional distillation from other gases. If 100 kg of silicon is reacted as shown in the figure below, how much trichlorosilane is produced? [15]



Solution:

Si overall mol balance:	3.560 = 0.3571 D + E	(1)
Cl overall mol balance:	A = D + 3 E	(2)
H overall mol balance:	A = 1.7142 D + E	(3)
(2) & (3): 2 E =	= 0.7142 D	
	E = 0.3571 D	(4)
(1) & (4): 3.56 =	0.3571 D + 0.3571 D	

D = 4.9846, E = 1.7899, A = 10.3246

СОМР	P. MW	
Н	1.01	
Si	28.09	
Cl₃	<u>106.35</u>	
-	135.45 kg/m	lol
	(135.45 kg HSiCl ₃)	(1.78 kg-mol)/(kg-mol HSiCl ₃) = 241.1 kg HSiCl₃

Question 5

- (a) Calculate the lower heating value of methane at 100 °C. [10]
- (b) Calculate the adiabatic flame temperature of C_3H_6 (g) at 1 atm when burned with 20% excess air and the reactants enter at 25 °C. [15]

Solution:

Or

(a)
$$CH_4(g) + 2 O_2(g) \rightarrow CO_2(g) + 2 H_2O(g)$$

. . . .

Basis: 1 g-mol CH₄

$$\Delta H_{rxn}(100^{\circ}C) = \sum \Delta H_{prod} - \sum \Delta H_{react}$$

$$\Delta H_{rxn}(100^{\circ}C) = \left[\left(\Delta h_{f,H20}^{\circ} \right) \times 2 + \left(\Delta h_{f,C02}^{\circ} \right) \times 1 + \left(\Delta h_{sensible,C02} \right) (1) + \left(\Delta h_{sensible,H20} \right) (2) \right]$$

$$- \left[\left(\Delta h_{f,CH4}^{\circ} \right) \times 1 + 0 \times 2 + \left(\Delta h_{sensible,CH4} \right) (1) + \left(\Delta h_{sensible,O2} \right) (2) \right]$$

$$= -822.66 \text{ kJ}$$

(b) $C_{3}H_{6}(g) + 4.5 O_{2}(g) \rightarrow 3 CO_{2}(g) + 3 H_{2}O(g)$

Basis: 1 g-mol C_3H_6 (g) Air in: required $O_2 = 4.5$ g-mol Excess 20% = 0.9 g-mol Total O_2 in = 4.5 + 0.9 = 5.4 g-mol N_2 in = 5.4 (79/21) = 20.31 g-mol

Reactants	g-mol	sens. Heat	heat-of-formation	
$C_{3}H_{6}$ (g) O_{2} (g) N_{2} (g)	1.0 5.4 20.31	0	20.41 0	<u> </u>
-2 (3)	20.51	U	0	<u>0</u>

Products: assume **T** = **200 K**, consult Table D-6.

<u>Comp.</u>	<u>g-mol</u>	sens. Heat	heat-of-formation	41171.73
CO ₂ (g) H ₂ O (g) O ₂ (g) N ₂ (g)	3 3 0.9 20.31	(92.466 - 0.912) (73.136 - 0.837) (59.914 - 0.732) (56.902 - 0.728)	-393.51 -241.826 0 0	<u>ΔH (kJ)</u> -905.87 -508.58 53.26 1140.89

Assume T :	= 2500 К			-220.30
$\frac{\text{Comp.}}{\text{CO}_2 (g)} \\ H_2 O (g) \\ O_2 (g) \\ N_2 (g) \\ P_2 H_2 H_2 H_2 \\ P_2 H_2 \\$	<u>g-mol</u> 3 3 0.9 20.31	<u>sens. Heat</u> (123.176 - 0.912) (98.867 - 0.837) (79.119 - 0.732) (75.060 - 0.728)	heat-of-formation -393.51 -241.826 0 0	<u>AH (kJ)</u> -813.74 -431.39 70.55 <u>1509.68</u> 335 11
Ky linoar in	torpolation	T . 3400 1/		

By linear interpolation, **T** = **2180 K**.

Question 6 (a)

One thousand pounds of 10% NaOH solution at 100 °F is to be fortified to 30% NaOH by adding 73% NaOH at 200 °F. How much 73% solution must be used? How much cooling must be provided so that the final temperature will be 70 $^{\circ}$ F? [15]

Solution:

Basis: 100 lb of NaOH at 100 $^{\circ}$ F

•	<u> Conc. </u>	lb NaOH	lh H ₂ O	Total
Initial Added Final	10% 73% 30%	100 0.73 m 100 + 0.73 m	900	1000
			0.27 m 900 + 0.27 m	m 1000 + m

(100.0 + 0.73 m)/(1000.0 + m) = 0.30So, m = 465 lb 73% NaOH added.

Reference state: Liquid water at 32 ^oF under its own vapor pressure ($\Delta H = 0$ Btu/lb) Take NaOH enthalpy values from H-x chart. $Q = \Delta H = \Delta H_{30\%} - [\Delta H_{10\%} + \Delta H_{73\%}]$

Conc.	Temp.	lb soln.	∆H. Btu/lb	AH Btu	
10	100 ⁰ F	1000	61	61 000	
73	200 [°] F	465	371	172 600	
30	70 ^o F	1465	37	54 200	
$Q = \Delta H =$: (54 200) – (6	51 000 + 17	2 000) = -179	400 Btu = H	leat removed

20.41

-220.30

Question 6 (b)

A rotary drier operating at atmospheric pressure dries 2000 lb/ day of wet grain at 70 $^{\circ}$ F, from a moisture content of 10% to 1% moisture. The air flow is counter current to the flow of grain, enters at 225 $^{\circ}$ F dry-bulb and 110 $^{\circ}$ F wet-bulb temperature, and leaves at 125 $^{\circ}$ F dry-bulb as saturated. Determine:

- (a) The humidity of the entering and leaving air
- (b) The water removal in pounds per hour
- (c) The daily product output in pounds per day

[2+4+4]



Solution:

- (a) The humidity of the entering air at 225 ^oF DB and 110 ^oF WB is obtained from the humidity chart as, Humidity = 0.031 lb H₂O/ lb dry air. Exit air humidity (saturated at 125 ^oF) = 0.0955 lb H₂O/ lb dry air
- (b) Basis: 1 hr

 $\frac{10 \text{ tons}}{\text{day}} \frac{|1 \text{ day}|}{|24 \text{ hr}|} \frac{2000 \text{ lb}}{|-835 \text{ lb/hr}}$ Water in = (0.1) (835) = 83.5 lb/hr Water out = $\frac{(0.9)(835) \text{ lb dry grain}}{|99 \text{ lb dry grain}} = 7.59 \text{ lb/hr}$ Pounds H₂O removed per hr = water in - water out = 83.5 - 7.59 = 75.9 lb H₂O/hr

(c) Product output =
$$\left[(0.9)(835) \frac{\text{lb dry grain}}{hr} + 7.59 \frac{\text{lb H}_2\text{O}}{hr} \right] \left(\frac{24 \text{ hr}}{1 \text{ day}} \right) = 18200 \text{ lb/day}$$

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CHE UC221 Chemical Process Calculations

<u>TEST - 2</u>

(Open Book)

DATE: 04-05-08

[10]

DURATION: 50 MINUTES

MAXIMUM MARKS: 60

Note: Attempt ALL questions. Draw a labeled flow diagram wherever necessary, mentioning therein all the known and unknown variables. *Text book by Himmelblau and Steam Tables are allowed.*

- 1 (a) At standard conditions, a gas that behaves as an ideal gas is placed in a 4.13 L container. By using a piston the pressure is increased to 31.2 psia, and the temperature is increased to 212 ^oF. What is the final volume occupied by the gas? [5]
- 1 (b) If a gas at 140 $^{\rm O}$ F and 30 in. Hg abs. has a molal humidity of 0.03 mole of H₂O per mole of dry air, calculate:
 - (a) The percentage humidity,
 - (b) The relative humidity (%), and
 - (c) The dew point of the gas (^oF).
- 2 (a) What is the enthalpy change that takes place when 3 kg of water at 101.3 kPa and 300 K are vaporized to 15 MPa and 800 K? [5]
- 2 (b) Two gram moles of nitrogen are heated from 50 $^{\circ}$ C to 250 $^{\circ}$ C in a cylinder. What is Δ H for the process? The heat capacity equation is: C_p = 27.32 + 0.6226 X 10⁻² T - 0.0950 X 10⁻⁵ T² where T is in Kelvin and C_p is in J/(g mol)($^{\circ}$ C) [5]
- 3 (a) Use the table of the heats of formation in Appendix F of the text book to calculate the standard heats of reaction per g-mol of the compounds produced in the following reactions: [3+3]
 (a) N₂ (g) + 3 H₂ (g) → 2 NH₃ (g)
 (b) Fe (s) + 1.5 Cl₂ (g) → FeCl₃ (s)
- 3 (b) The chemist for a gas company finds a gas analyses 9.2% CO₂, 0.4% C_2H_4 , 20.9% CO, 15.6% H_2 , 1.9% CH₄, and 52.0% N₂. What would the chemist report as the gross heating value of the gas? [9]

4 (a) The following enthalpy changes are known for reactions at 25 ^oC in the standard thermo-chemical state:

$C_{3}H_{6}(g) + H_{2}(g) \rightarrow C_{3}H_{8}(g)$	ΔH^{o} (kJ) = -124.0
$C_{3}H_{8}(g) + 5O_{2}(g) \rightarrow 3CO_{2}(g) + 4H_{2}O(I)$	$\Delta H^{o}(kJ) = -2220.0$
$H_2(g) + \frac{1}{2}O_2(g) \rightarrow H_2O(I)$	ΔH^{o} (kJ) = -286.0
$H_2O(I) \rightarrow H_2O(g)$	ΔH^{o} (kJ) = -44.0
$C + O_2(g) \rightarrow CO_2(g)$	$\Delta H^{o}(kJ) = -393.5$

Calculate heat of formation of propylene.

[5]

4 (b) In human body, glucose reacts as $C_6H_{12}O_6$ (glucose) + 6 $O_2 \rightarrow 6$ H₂O (l) + 6 CO₂ (g) How many liters of O₂ would be required for the reaction of one gram of glucose if the conversion is 90% complete in human body? How many kJ/g of energy from glucose will be produced in the body? Data given: Standard heat of formation (glucose) = -1260 kJ/g-mol glucose, Assume the reaction takes place at 25 °C and 1 atm. Assume body temperature to be 37 °C. [15]

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CHE UC221 Chemical Process Calculations

TEST - 1 (Closed Book)

DURATION: 60 MINUTES

DATE: 23-03-08 MAXIMUM MARKS: 75

Note: Attempt ALL questions. Draw a labeled flow diagram wherever necessary, mentioning therein all the known and unknown variables.

- 1 (a) A drain cleaner contains 5.00 kg of water and 5.00 kg of NaOH. What are the mass fraction and mole fraction of each component in the drain cleaner container. Given molecular weight of NaOH = 40. [1+2=3]
- 1 (b) Given a 50-kg gas mixture containing 10.0% H₂, 40.0% CH₄, 30.0% CO, and 20.0% CO₂. What is the average molecular weight of the gas? [3]
- 1 (c) How is specific gravity defined for liquids and for gases? [4]
- 2 Methane is burned to form CO_2 and water in a batch reactor: $^{-}CH_4 + 2 O_2 \rightarrow CO_2 + 2 H_2O$ The feed to the reactor and the products obtained are shown in the flow chart Find out
- a) How much CH₄ was consumed? What is fractional conversion of CH_4 ?
- b) How much oxygen was consumed? What is the fractional conversion of oxygen?
- c) What is the percent excess oxygen used?

[3+3+4=10]

100 mol CH_ $250 \text{ mol } O_2$

Reactor

40 mol CH \rightarrow 130 mol O₂ $60 \text{ mol } \text{CO}_2$ 120 mol H₂O

3 A limestone analysis is given as C- CO

CaCO ₃	92.89%
MgCO₃	5.41%
Insoluble	1.70%

Find out

a) How many kg of calcium oxide can be made from 5000 kg of this limestone?

b) How many kg of CO_2 can be recovered per kg of limestone?

c) How many kg of limestone are needed to make 1000 kg of lime? [15]

1

Antimony is obtained by heating pulverized stibnite (Sb_2S_3) with scrap iron and drawing off the molten antimony from the bottom of the reaction vessel: $Sb_2S_3 + 3 \text{ Fe} \rightarrow 2 \text{ Sb} + 3 \text{ FeS}$ Suppose that 0.60 kg of stibnite and 0.25 kg.

Suppose that 0.60 kg of stibnite and 0.25 kg of iron turnings are heated together to give 0.20 kg of Sb metal. Determine

- a) The limiting reactant,
- b) The percent of excess reactant,
- c) The degree of completion (fraction),

d) The yield.

Given: molecular weights: Fe = 55.85, Sb = 121.8, S = 32.0 [3+4+4+4=15]

- 5 (a) A cellulose solution contains 5.2% cellulose by weight in water. How many kg of 1.2% solution are required to dilute 100 kg of 5.2% solution to 4.2%? [5]
- 5 (b) A cereal product containing 55% water is made at the rate of 500 kg/h. you need to dry this product so that it contains only 30% water. How much water has to be evaporated per hour? [5]
- 6 16 kg of methane is burned with 300 kg air. Find out the composition of flue gas in mole percent. [15]
